

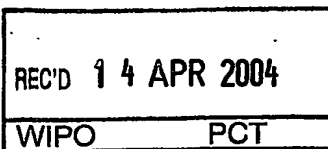


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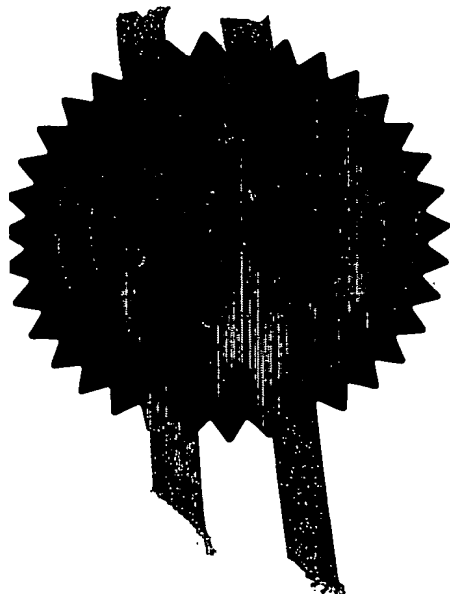


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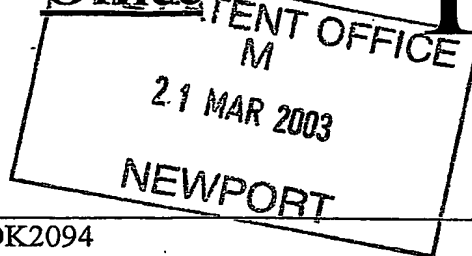


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1. Your reference **21 MAR 2003**

CDK2094

2. Patent application number  
(The Patent Office will fill in this)

**0306531.5**

21 MAR 2003 E794189-10 D02806  
P01/7700 0.00-0306531.5

3. Full name, address and postcode of the or of each applicant (underline all surnames)

RHODIA CONSUMER SPECIALTIES LIMITED  
Oak House  
Reeds Crescent  
Watford  
Hertfordshire, WD24 4QP.

Patents ADP number (if you know it)

If the applicant is a corporate body, give the country/state of its incorporation

7870322006

4. Title of the invention

FORMULATION FOR CORROSION AND SCALE  
INHIBITION

5. Name of your agent (if you have one)

Barker Brettell

"Address for service" in the United Kingdom to which all correspondence should be sent (including the postcode)

138 Hagley Road  
Edgbaston  
Birmingham  
B16 9PW

Patents ADP number (if you know it)

7442494002

6. If you are declaring priority from one or more earlier patent applications, give the country and the date of filing of the or of each of these earlier applications and (if you know it) the or each application number

Country

Priority application number  
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Date of Filing  
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7. If this application is divided or otherwise derived from an earlier UK application, give the number and the filing date of the earlier application

Number of earlier application

Date of filing  
(day/month/year)

8. Is a statement of inventorship and of right to grant of a patent required in support of this request (Answer 'Yes' if:

Yes

a) any applicant named in part 3 is not an inventor, or  
b) there is an inventor who is not named as an applicant, or  
c) any named applicant is a corporate body.  
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# Patents Form 1/77

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Description 6 + 6 ✓

Claim(s) 3 + 3 ✓

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Statement of inventorship and right to grant of a patent (*Patents Form 7/77*) -

Request for preliminary examination 1 ✓  
(*Patents Form 9/77*)

Request for substantive examination -  
(*Patents Form 10/77*)

Any other documents -  
(*please specify*)

11. I/We request the grant of a patent on the basis of this application.

Signature *Barker Brettell* Date

**Barker Brettell**

20 March 2003

12. Name and daytime telephone number of person to contact in the United Kingdom

Colin D. Kinton

Tel: 0121 456 1364

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# FORMULATION FOR CORROSION AND SCALE INHIBITION

The present invention relates to a method of preventing or alleviating the problems associated with metal sulphide deposits and to novel formulations for use in such a method.

Tetrakis (hydroxyorgano) phosphonium salts (hereinafter THP<sup>+</sup> salts), especially tetrakis (hydroxymethyl) phosphonium sulphate (hereinafter THPS) are widely used as metal sulphide dissolver/dispersers within aqueous systems and especially those systems associated with oilfields.

When THPS is used in oilfields, it is typically applied in concentrations of up to 30%, together with an ammonium salt to improve performance. This combination of THPS and an ammonium salt, together with high temperatures that can be experienced in oilfield applications, can be corrosive to mild steel and other metal components.

It is an aim of the present invention to ameliorate the above problems of corrosion by THP<sup>+</sup> salts when used in aqueous systems.

20

Accordingly, the present invention, in a first aspect, provides a formulation for use in the treatment of corrosion and metal sulphide scale deposits in aqueous systems, said formulation comprising a THP<sup>+</sup> salt (as hereinbefore defined) and a thio-substituted compound.

25

The metal sulphide scale may be iron sulphide. Alternatively, the metal sulphide may be lead sulphide or zinc sulphide or a combination thereof. The iron sulphide may be Troilite (FeS) or Pyrite (FeS<sub>2</sub>). Alternatively, the iron sulphide may be Mackinawite (Fe<sub>9</sub>S<sub>8</sub>) or Pyrrhotite (Fe<sub>7</sub>S<sub>8</sub>).

30

The anion of the THP<sup>+</sup> salt should be compatible with the aqueous system. Preferred anions include sulphate, chloride, phosphate, bromide, fluoride, carbonate, citrate, lactate, tartrate, borate, silicate, formate and acetate. The anion should make the THP<sup>+</sup> salt water-soluble.

5

The thio-substituted compound is preferably thioglycollic acid (CAS No 68-11-1). Alternatively, the thio-substituted compound is selected from the group consisting of thio-substituted carboxylic acids or salts e.g. thiolactic acid, thiomalic acid and mercaptopyruvic acid; thio-substituted  
10 sulphonic acids e.g. mercaptoethane sulphonic acid; mercaptoalcohols e.g. mercaptoethanol; alkyl or aryl thiols (substituted and unsubstituted) e.g. mercaptoethane and thiocresol; and thio-substituted heterocyclic compounds e.g. mercaptomethylimidazole, mercaptothiazoline and mercaptopyridine.

15

The formulation may further include a surfactant. The surfactant is preferably a cationic surfactant, for example quaternary ammonium compounds, N-alkylated heterocyclic compounds or quaternised amido-amines. Anionic, amphoteric or non-ionic surfactants may also be used.

20 The use of ammonium salts may be substituted for an aminomethane phosphonate.

The formulation according to the invention is particularly useful in the prevention of corrosion of mild steel, copper and aluminium.

25

The present invention also provides, in a second aspect, a method for treatment of an aqueous system containing or in contact with a metal sulphide scale while concomitantly inhibiting the corrosion of surfaces in contact with said aqueous system, which method comprises the addition to  
30 said aqueous system of a scale and corrosion inhibiting amount of a formulation in accordance with the first aspect of the invention.

The aqueous system is preferably one used in enhanced oil recovery. Alternatively, the aqueous system is one used in industrial water systems, paper manufacturing systems and any aqueous system wherein corrosion  
5 caused by  $\text{THP}^+$  salts occurs.

The present invention also provides, in a third aspect, a formulation consisting essentially of the reaction product of a  $\text{THP}^+$  salt a thio-substituted compound, wherein the ratio of said  $\text{THP}^+$  salt and said  
10 thio-substituted compound is between 1:1 and 750:1.

The formulation as described in the first aspect is preferably used in an effective amount up to 30% by weight as  $\text{THP}^+$ . The amount used will vary by application but it may also be effectively used for low level  
15 applications e.g. 1 to 10000ppm as a  $\text{THP}^+$  salt or in high level applications as 1 to 30% as a  $\text{THP}^+$  salt. In the second aspect  $\text{THP}^+$  is preferably used in an effective amount of up to 30% by weight as a  $\text{THP}^+$  salt with the co-addition of a thio-substituted compound in an effective amount of between 0.1 to 10000 ppm in relation to the volume of the  
20 system being treated.

The ratio of  $\text{THP}^+$  to the thio-substituted compound in the formulation is typically in the range 1:1 to 750:1, more preferentially 15:1 to 300:1, most preferably 75:1 to 150:1.  
25

The present invention will be illustrated, merely by way of example, as follows.

#### Example 1.

30 Blank Experiment: A 100ml solution of 20% THPS (26.6g TOLCIDE® PS75) and 1g ammonium chloride in synthetic seawater was placed in a

- 120ml screw-top jar. A pre-weighed mild steel coupon was immersed in the solution. The jar was then stored in a 50°C oven for 48 hours. After this time the coupon was cleaned by gentle scrubbing in water, washed with acetone and dried in the oven. The coupons were then reweighed and
- 5 the corrosion rate calculated according to the equation:

$$\text{Rate} = \frac{K \times W}{A \times T \times d}$$

- 10  $W$  = Weight loss in g (to 0.1mg)

$A$  = Area in  $\text{cm}^2$  (to 0.01  $\text{cm}^2$ )

$T$  = Time of exposure in hours

$d$  = Density in  $\text{g/cm}^3$

- 15  $K$  is a constant defined by the units in which the corrosion rate is required. For example:

Units

$K$

Mpy - mils per year

$3.45 \times 10^6$

20

This experiment was repeated with various levels of corrosion inhibitor added to the blank solution. The results are shown in the table below:

TABLE

Experiment	Corrosion Rate mpy
Blank	208
Blank + 5000ppm Inhibitor A	77
Blank + 5000ppm Inhibitor B	197
Blank + 5000ppm Inhibitor C	116
Blank + 5000ppm Inhibitor D	132
Blank + 5000ppm Inhibitor E	88
Blank + 5000ppm Inhibitor F	86
Blank + 5000ppm Inhibitor G	28
Blank + 1% Inhibitor E	78
Blank + 1% Inhibitor F	74
Blank + 1% Inhibitor G	14
Blank + 100ppm Thioglycollic acid	47
Blank + 1000ppm Thioglycollic acid	38
Blank + 1000ppm Thioglycollic acid + 1000ppm quaternary ammonium chloride	23
Blank + 2800ppm Thioglycollic acid + 1000ppm quaternary ammonium chloride	17

5

**Blank** – A solution consisting of 20% THPS and 1% ammonium chloride in synthetic seawater.

**Inhibitor A** – Commercially available corrosion inhibitor comprising ethoxylated ammonium chloride, dibutyl thiourea and ethoxylated fatty acid.

10



**Inhibitor B** - Commercially available corrosion inhibitor comprising polyoxyethylene 2-ethylhexyl ether phosphate.

**Inhibitor C** - Oilfield corrosion inhibitor comprising fatty acids and Tall oil reaction products with diethylene triamine.

- 5 **Inhibitor D** - Commercially available corrosion inhibitor comprising a phosphonocarboxylic acid.

**Inhibitor E** - Standard commercially available oilfield corrosion inhibitor based on an amine alkoxylate.

- 10 **Inhibitor F** - Standard commercially available oilfield corrosion inhibitor comprising an amine ethoxylate and a quaternary ammonium chloride.

**Inhibitor G** - Standard commercially available oilfield corrosion inhibitor comprising thioglycolic acid and a quaternary ammonium chloride.

## CLAIMS

1. A formulation for use in the treatment of corrosion and metal sulphide scale deposits in aqueous systems, said formulation comprising a  
5 THP<sup>+</sup> salt (as hereinbefore defined) and a thio-substituted compound.
2. A formulation as claimed in Claim 1 in which the metal sulphide scale is iron sulphide.
- 10 3. A formulation as claimed in Claim 1 in which the metal sulphide scale is lead sulphide.
4. A formulation as claimed in Claim 1 in which the metal sulphide scale is zinc sulphide.
- 15 5. A formulation as claimed in any one of the preceding claims in which the THP<sup>+</sup> salt comprises an anion selected from the group consisting of sulphate, chloride, phosphate, bromide, fluoride, carbonate, citrate, lactate, tartrate, borate, silicate, formate and acetate.
- 20 6. A formulation as claimed in any one of Claims 1 to 5 in which the thio-substituted compound is selected from the group consisting of thio-substituted carboxylic acids or salts; thio-substituted sulphonic acids; substituted and unsubstituted alkyl and aryl thiols; thio-substituted  
25 heterocyclic compounds; and mercaptoethanols.
7. A formulation as claimed in Claim 6 in which the thio-substituted compound is thioglycollic acid.
- 30 8. A formulation as claimed in any one of the preceding claims in which said formulation further includes a surfactant.

9. A formulation as claimed in Claim 8 in which the surfactant is a cationic surfactant.
- 5 10. A formulation as claimed in Claim 9 in which the cationic surfactant is selected from the group consisting of quaternary ammonium compounds, N-alkylated heterocyclic compounds, quaternised amido-amines, and amino methane phosphonate.
- 10 11. A formulation as claimed in Claim 8 in which the surfactant is selected from the group consisting of anionic, amphoteric and non-ionic surfactants.
12. The use of a formulation as claimed in any one of the preceding  
15 claims for treating corrosion of mild steel, copper or aluminium.
13. A method for treatment of an aqueous system containing or in contact with a metal sulphide scale while concomitantly inhibiting the corrosion of surfaces in contact with said aqueous system, which method  
20 comprises the addition to said aqueous system of a scale and corrosion inhibiting amount of a formulation in accordance with any one of Claims 1 to 11.
14. A method according to Claim 13 in which the aqueous system is  
25 used in enhanced oil recovery.
15. A method as claimed in Claim 13 in which the aqueous system is used in industrial water systems.
- 30 16. A method as claimed in Claim 13 in which the aqueous system is used in paper manufacturing systems.

17. A formulation consisting essentially of the reaction product of a THP<sup>+</sup> salt (as hereinbefore defined) and a thio-substituted compound, wherein the ratio of said THP<sup>+</sup> salt and said thio-substituted compound is between 1:1 and 750:1.
18. A method as claimed in any one of Claims 13 to 16 in which the THP<sup>+</sup> salt is added to the aqueous system in an effective amount of up to 30% by weight.
19. A formulation as claimed in any one of Claims 1 to 11 in which the ratio of the THP<sup>+</sup> salt to the thio-substituted compound is between 1:1 and 750:1.
20. A formulation substantially as described herein with reference to the accompanying example.
21. A method substantially as described herein with reference to the accompanying example.

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